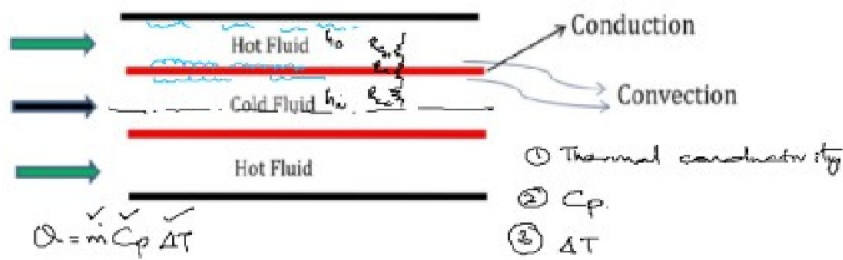




DEPARTMENT OF MECHANICAL ENGINEERING, 16ME306/ Heat and Mass Transfer – UNIT III -
PHASE CHANGE HEAT TRANSFER AND HEAT EXCHANGERS

Topic - Types of Heat Exchangers- Heat Exchanger Analysis- LMTD Method

Heat exchangers are the devices that facilitate heat transfer between two (or) more fluids at different temperatures, while keeping them from mixing (or) without mixing. Heat transfer in heat exchanger involves convection in each fluid and conduction through the wall separating the fluids.



Examples: Shell and tube heat exchanger.

Boilers.

Cooling towers

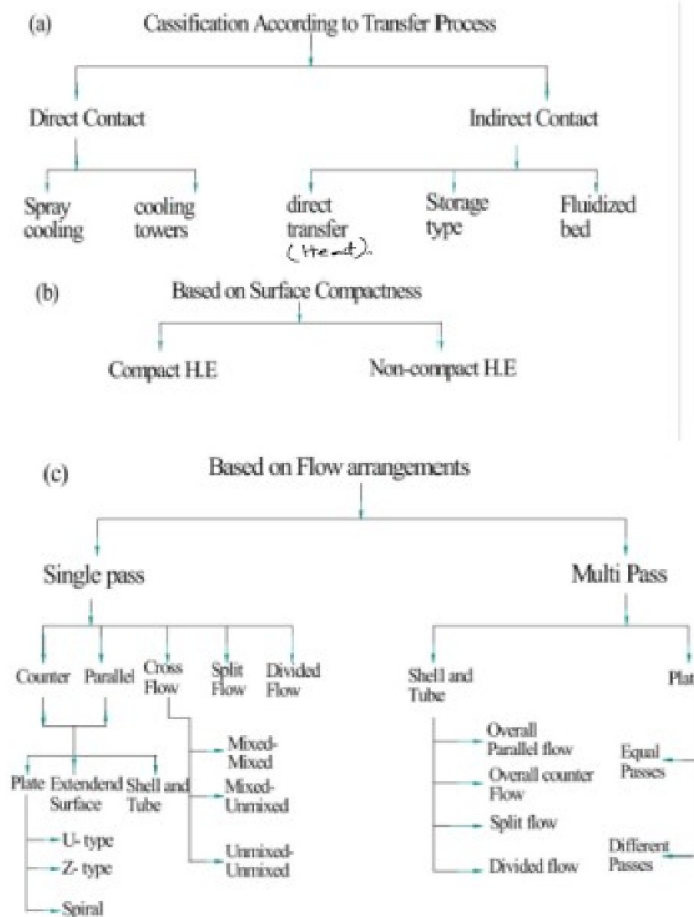
Car radiators etc.,



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Classification of Heat Exchangers:





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Heat transfer analysis of heat exchangers

To design or predict the performance, the fluid temperatures, overall heat transfer coefficient and surface area parameters are to be evaluated. They are modelled as steady-flow devices. The methods used for analysis are:

1) LMTD approach (log mean Temp difference)
Known \rightarrow Temperatures, Mass flow rates, overall heat transfer coefficient.

Calculate the size of the heat exchanger $\frac{D_o L_o}{D_i L_i}$

2) ε-NTU approach: (Number of Transfer units).
Known \rightarrow either inlet or outlet temperatures, size.

Type and size of heat exchanger.

Calculate the missing temperatures, Load on the heat exchanger.

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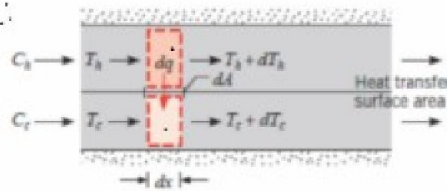
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LMTD for parallel flow heat exchanger

Heat capacity:

$$C_h = \dot{m}_h C_{ph}$$

$$C_c = \dot{m}_c C_{pc}$$

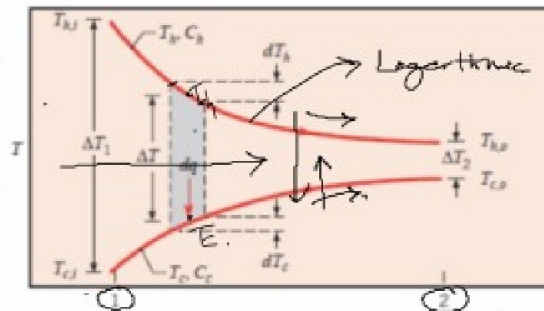


i = inlet //
o = outlet //

Temp Vs dist.

$$\Delta T_1 = T_{hi} - T_{ci}$$

$$\Delta T_2 = T_{ho} - T_{co}$$



$T_{hi} > T_{ho}$
 $T_{co} > T_{ci}$

Assumptions: [Both parallel & counter flow HEs] ~~X~~

- 1) Steady flow.
- 2) KE and PE are neglected.
- 3) Thermo physical properties are constant over the entire length of HE.
- 4) No heat loss to the surrounding (adiabatic)
- 5) Heat transfer coefficient is constant over the entire length.



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Let, $A =$ Surface area in m^2 .

$\dot{m}_c, \dot{m}_h =$ Mass flow rate in kg/s .

$\Delta T = T_h - T_c =$ Local temperature difference b/w
hot and cold fluids in $^{\circ}C$ (or) K .

$U =$ Overall heat transfer coefficient.

Applying the energy balance: (hot & cold fluid)

$$Q = \underbrace{\dot{m}_c}_{C_c} C_p (T_{c0} - T_{c1}) = \underbrace{\dot{m}_h}_{C_h} C_p (T_{h1} - T_{h0}) \rightarrow (1)$$

Heat capacities are.

$$C_c = \dot{m}_c C_p \text{ and } C_h = \dot{m}_h C_p. \rightarrow (2)$$

Rate of heat transfer $\dot{d}Q$ from the hot to
the cold fluid through an elemental area $\dot{d}A$
is given by:

$$dQ = U \cdot dA \cdot dT \rightarrow (3) \quad [Q = UA \Delta T].$$

Also, dQ should be equal to the heat given up
by the hot fluid (or) gained by the cold fluid
flowing through an elemental area $\dot{d}A$, is.

$$dQ = \dot{m}_c C_p dT_c - \dot{m}_h C_p dT_h \rightarrow (4)$$

[-ve sign due to heat lost by the hot fluid] \otimes



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Rewriting the above equations

$$dT_c = \frac{dQ}{\dot{m}_c C_{pc}} \text{ and } dT_h = -\frac{dQ}{\dot{m}_h C_{ph}} \rightarrow \textcircled{5}$$

If, $\Delta T_1 = T_{hi} - T_{ci}$ and $\Delta T_2 = T_{ho} - T_{co}$, then.

$$dT_h - dT_c = -\frac{dQ}{\dot{m}_h C_{ph}} - \frac{dQ}{\dot{m}_c C_{pc}}$$

$$d(T_h - T_c) = -dQ \left[\frac{1}{\dot{m}_h C_{ph}} + \frac{1}{\dot{m}_c C_{pc}} \right] \rightarrow \textcircled{6}$$

Substitute $\textcircled{5}$ in $\textcircled{6}$, we get.

$$d(T_h - T_c) = -U dA dT \left[\frac{1}{\dot{m}_h C_{ph}} + \frac{1}{\dot{m}_c C_{pc}} \right]$$

Integrating between inlet and outlet.

$$\int_{\text{inlet}=\Delta T_1}^{\text{outlet}=\Delta T_2} \frac{d(T_h - T_c)}{dT} = - \int_{\text{inlet}}^{\text{out}} U \cdot dA \left[\frac{1}{\dot{m}_h C_{ph}} + \frac{1}{\dot{m}_c C_{pc}} \right]$$

$$\ln \left(\frac{T_{ho} - T_{co}}{T_{hi} - T_{ci}} \right) = -UA \left[\frac{1}{\dot{m}_h C_{ph}} + \frac{1}{\dot{m}_c C_{pc}} \right]$$

Substituting for $\dot{m}_h C_{ph}$ & $\dot{m}_c C_{pc}$ from $\textcircled{1}$, we get.

$$\ln \left(\frac{T_{ho} - T_{co}}{T_{hi} - T_{ci}} \right) = -UA \left[\frac{T_{hi} - T_{ho}}{Q} + \frac{T_{co} - T_{ci}}{Q} \right]$$



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$$\ln \left(\frac{T_{h0} - T_{c0}}{T_{hi} - T_{ci}} \right) = -\frac{UA}{Q} \left[T_{hi} - T_{h0} + T_{c0} - T_{ci} \right]$$

Rearranging the terms.

$$\ln \left(\frac{T_{h0} - T_{c0}}{T_{hi} - T_{ci}} \right) = -\frac{UA}{Q} \left[(T_{hi} - T_{ci}) - (T_{h0} - T_{c0}) \right]$$

$$\ln \left(\frac{T_{h0} - T_{c0}}{T_{hi} - T_{ci}} \right) = \frac{UA}{Q} \left[(T_{h0} - T_{c0}) - (T_{hi} - T_{ci}) \right]$$

$$\therefore Q = \frac{UA \left[(T_{h0} - T_{c0}) - (T_{hi} - T_{ci}) \right]}{\ln \left(\frac{T_{h0} - T_{c0}}{T_{hi} - T_{ci}} \right)}$$

$$Q = \frac{UA (\Delta T_2 - \Delta T_1)}{\ln \left(\frac{\Delta T_2}{\Delta T_1} \right)}$$

[OR]

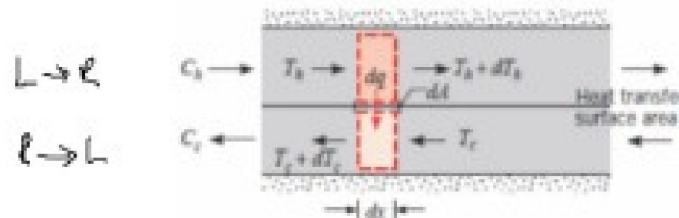
$$Q = \frac{UA (\Delta T_1 - \Delta T_2)}{\ln \left(\frac{\Delta T_1}{\Delta T_2} \right)}$$

→ Logarithmic mean
temperature diff
(LMTD)

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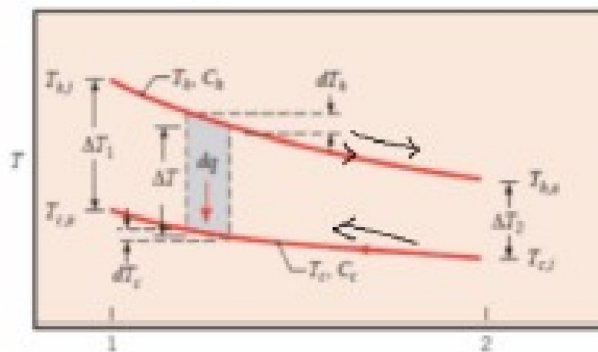
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LMTD for Counter flow heat exchanger.



$$\Delta T_1 = T_{h1} - T_{c2}$$

$$\Delta T_2 = T_{h2} - T_{c1}$$



Let, A = Surface area in m^2 .

\dot{m}_c, \dot{m}_h = Mass flow rate in kg/s .

$\Delta T = T_h - T_c$ = Local temperature difference b/w hot and cold fluids in $^{\circ}C$ (or) K .

U = Overall heat transfer coefficient.

Applying the energy balance: (hot & cold fluids)

$$Q = \underbrace{\dot{m}_c}_{C_c} C_p (T_{c2} - T_{c1}) = \underbrace{\dot{m}_h}_{C_h} C_p (T_{h1} - T_{h2}) \rightarrow \textcircled{1}$$

Heat capacities are.

$$C_c = \dot{m}_c C_p \text{ and } C_h = \dot{m}_h C_p. \rightarrow \textcircled{2}$$



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Rate of heat transfer dQ from the hot to the cold fluid through an elemental area dA is given by;

$$dQ = U \cdot dA \cdot dT \rightarrow \textcircled{2} \quad [Q = UA \Delta T].$$

Also, dQ should be equal to the heat given up by the hot fluid (or) gained by the cold fluid flowing through an elemental area dA , is.

$$\textcircled{x} \quad dQ = -\dot{m}_c C_{pc} dT_c = \dot{m}_h C_{ph} dT_h \rightarrow \textcircled{4}$$

$\left[\begin{array}{l} \text{-ve sign due to heat lost for hot fluid.} \\ \text{-ve sign. due to opposite direction for cold fluid} \end{array} \right]$

Rearranging the above equations

$$dT_c = \frac{-dQ}{\dot{m}_c C_{pc}} \quad \text{and} \quad dT_h = \frac{-dQ}{\dot{m}_h C_{ph}} \rightarrow \textcircled{5}$$

If, $\Delta T_1 = T_{hi} - T_{co}$ and $\Delta T_2 = T_{ho} - T_{ci}$, then.

$$dT_h - dT_c = -\frac{dQ}{\dot{m}_h C_{ph}} + \frac{dQ}{\dot{m}_c C_{pc}}$$

$$d(T_h - T_c) = -dQ \left[\frac{1}{\dot{m}_h C_{ph}} - \frac{1}{\dot{m}_c C_{pc}} \right] \rightarrow \textcircled{6}$$



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Substituting (E) in (E), we get.

$$d(T_h - T_c) = -U dA dT \left[\frac{1}{\dot{m}_h C_{ph}} - \frac{1}{\dot{m}_c C_{pc}} \right]$$

Integrating between inlet and outlet.

$$\int_{\text{inlet}=\Delta T_1}^{\text{outlet}=\Delta T_2} \frac{d(T_h - T_c)}{dT} = - \int_{\text{inlet}}^{\text{out}} U \cdot dA \left[\frac{1}{\dot{m}_h C_{ph}} - \frac{1}{\dot{m}_c C_{pc}} \right]$$

$$\ln \left(\frac{T_{ho} - T_{ci}}{T_{hi} - T_{co}} \right) = -UA \left[\frac{1}{\dot{m}_h C_{ph}} - \frac{1}{\dot{m}_c C_{pc}} \right]$$

Substituting for $\dot{m}_h C_{ph}$ & $\dot{m}_c C_{pc}$ from (D), we get

$$\ln \left(\frac{T_{ho} - T_{ci}}{T_{hi} - T_{co}} \right) = -UA \left[\frac{T_{hi} - T_{ho}}{Q} - \frac{T_{co} - T_{ci}}{Q} \right]$$

$$\ln \left(\frac{T_{ho} - T_{ci}}{T_{hi} - T_{co}} \right) = -\frac{UA}{Q} \left[T_{hi} - T_{ho} - T_{co} + T_{ci} \right]$$

Rearranging the terms.

$$\ln \left(\frac{T_{ho} - T_{ci}}{T_{hi} - T_{co}} \right) = -\frac{UA}{Q} \left[(T_{hi} - T_{co}) - (T_{ho} - T_{ci}) \right]$$



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$$\ln \left(\frac{T_{ho} - T_{ci}}{T_{hi} - T_{co}} \right) = \frac{UA}{Q} \left[(T_{ho} - T_{ci}) - (T_{hi} - T_{co}) \right]$$

$$\therefore Q = \frac{UA \left[(T_{ho} - T_{ci}) - (T_{hi} - T_{co}) \right]}{\ln \left(\frac{T_{ho} - T_{co}}{T_{hi} - T_{ci}} \right)}$$

$$Q = UA \frac{(\Delta T_2 - \Delta T_1)}{\ln \left(\frac{\Delta T_2}{\Delta T_1} \right)}$$

$$[OR] \quad Q = UA \frac{(\Delta T_1 - \Delta T_2)}{\ln \left(\frac{\Delta T_1}{\Delta T_2} \right)}$$

*Logarithmic mean
temperature diff
(LMTD)*

⊗ Note:

Even though the mathematic expression for both parallel and counter flow heat exchanger looks similar, the temperature differences (ΔT) at the inlet and outlet are different.



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3. MIT open courseware - <https://ocw.mit.edu/courses/mechanical-engineering>

Other web sources