

13/9/22

## Properties of Pure Substance

### Steam

Steam is a vapour. It is used as the working substance in the operation of steam engines and steam turbines. A vapour is a partially evaporated liquid carrying in it particles of liquid and it can be liquefied by reducing pressure or temperature. Steam as a vapour would not obey the laws of perfect gases unless it is in a highly dried condition. Steam in such a dried state is known as superheated steam and it is assumed to behave like a perfect gas when highly superheated.

### Properties of steam

(\*) Pressure

(\*) Temperature

(\*) Specific volume

(\*) Enthalpy

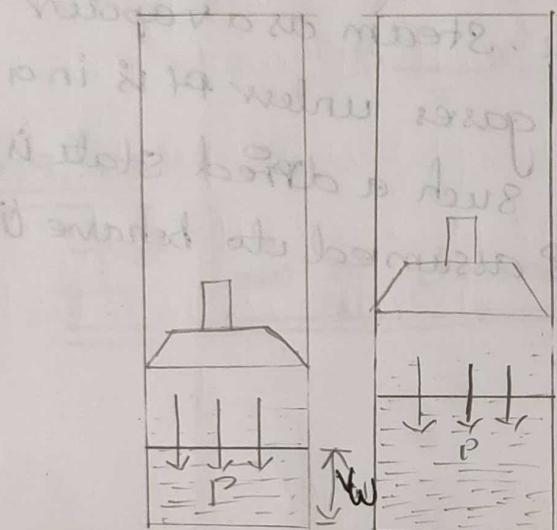
(\*) Entropy

Pressure, temperature and volume can be given their actual absolute values, whereas enthalpy and entropy are purely relative quantities. They are measured relatively from convenient datum condition of the water at  $0^\circ\text{C}$ . Thus, the enthalpy, the internal energy and the entropy of water at  $0^\circ\text{C}$  are assumed to be zero. All their values measured above this temperature are considered positive and those measured below are taken as negative.

## Formation of steam at constant Pressure

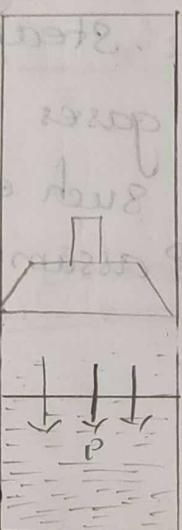
Consider a cylinder fitted with frictionless piston which may be loaded to any desired pressure  $P$  bar as shown.

### Properties of Steam



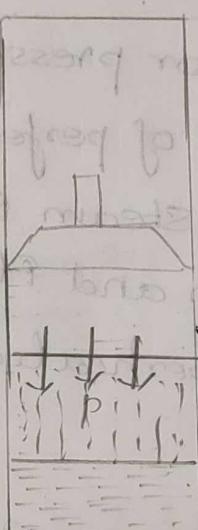
All water  
at  $0^{\circ}\text{C}$

(a)



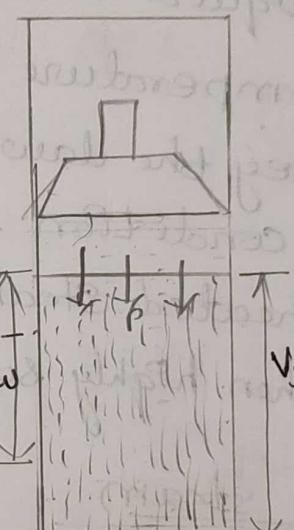
All water  
at  $t_s$

(b)



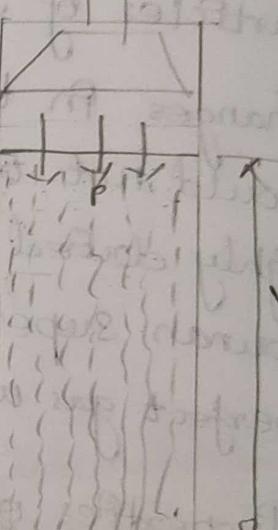
Half water  
& half steam  
at  $t_s$

(c)



All steam  
at  $t_s$

(d)



All steam  
at  $t_s$  up.  
 $h$

(e)

(i) The kilogram of water initially at temperature  $0^{\circ}\text{C}$  in the cylinder under the piston and the piston exerts a constant pressure  $P$  bar.

(ii) Let the area of the piston be one square metre and the volume of one kilogram of water be  $V_w \text{ m}^3$ .

(iii) The length  $P$  in the cylinder occupied by water will be  $V_w \text{ m}$ . Now let heat be supplied to the water in the cylinder.

(iv) The temperature of water will rise when sensible enthalpy is supplied. The rise in temperature at which water boils depends upon the pressure  $P$ .

(v) The given pressure there is one kgof defn to boiling point. The boiling point is called the saturation temperature ( $t_s$ ) or the temperature of steam formation. Water boils at  $99.63^\circ\text{C}$  when the pressure on  $P_1$  is 1 bar and at  $184.09^\circ\text{C}$  when the pressure on  $P_1$  is 11 bar.

(vi) The water will expand slightly during the rise of temperature. The increase in volume of water causes the piston to move up slightly as shown.  $\frac{P_1 V}{T_1} = \frac{P_2 V_2}{T_2}$ . The work done in moving the piston against the pressure  $P$ . This work however is only a small portion of the heat added to water during the rise in temperature and may be neglected in general.

(vii) The next stage, the actual production of steam. If the heating of this one kilogram of water is continued after the boiling is reached. It will be noticed that there is no further increase in temperature.

(viii) A mixture of steam and water is called wet steam. If the heating of this wet steam is further continued and as soon as last particle of water in suspension in wet disappears, the steam produced is known as dry saturated steam.

(ix) The process of formation of steam is completed. The water is entirely evaporated and the volume of steam below the piston is  $V_s \text{ m}^3$ . The piston will rise to accommodate this increased volume and will occupy length  $V_s \text{ m}$  of the cylinder.

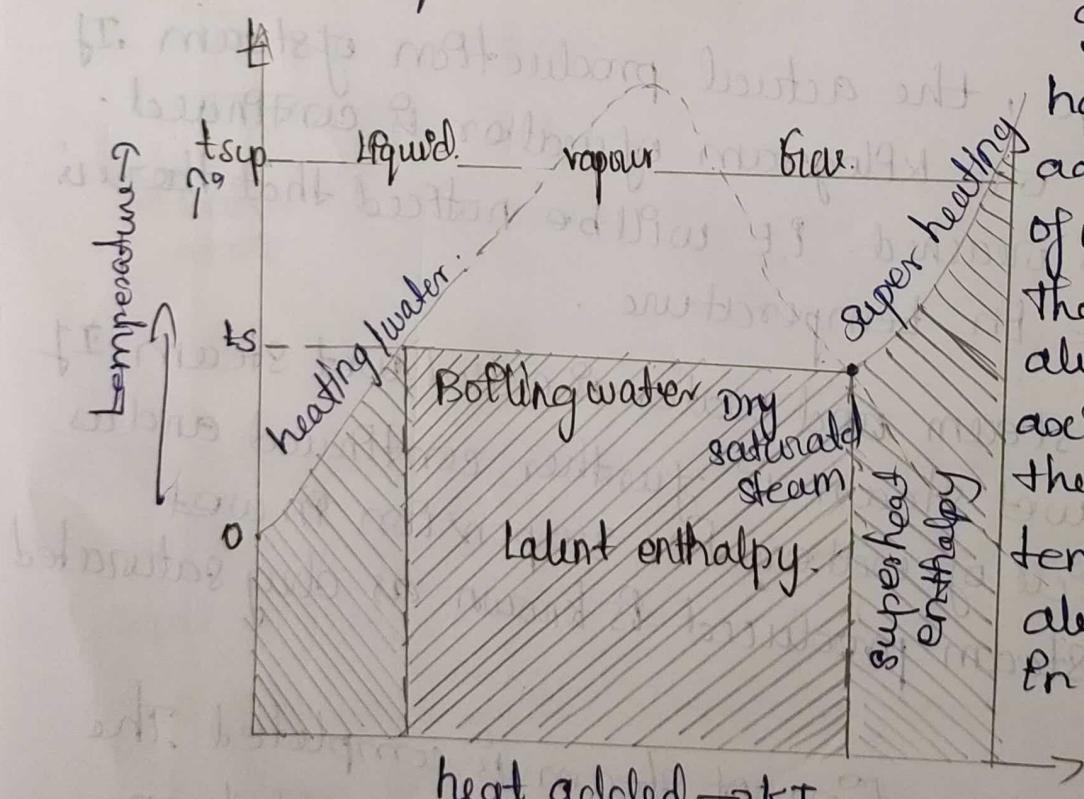
The workdone on the piston during the change of volume of the steam from  $V_1$  to  $V_s$ .

$$\text{workdone} = \frac{10^5 p(v_s - v_w)}{10^3} \text{ kJ} \quad \text{where } p \rightarrow \text{is the pressure in bar.}$$

If  $p$  is in kPa, then the above expression is written

$$\text{workdone} = p(v_s - v_w) \text{ kJ}$$

Finally the ~~it~~ further heat is added to one kilogram of dry steam in the cylinder at the constant pressure, the temperature of steam will rise and there will be further increase in volume of steam as. This steam produced is known as superheated steam.



graphically that what happens when heat is added to one kilogram of water. Initially at  $0^\circ\text{C}$  the heat added is plotted along the horizontal axis in kJ units while the corresponding temperature are plotted along the vertical axis in centigrade units.

During the first stage of heating the temperature of water will begin to rise until the water will begin to rise until the water boils at a temperature which depends upon the pressure in the cylinder. After the boiling temperature is reached, steam begins to be formed during which time the temperature remains constant.

Enthalpy: For reasons too long to explain here, the term heat content is not recommended for use in thermodynamics. The terms formerly known as "heat of water" (sensible heat), "heat of evaporation" (latent heat) and "total heat of steam" are now known as the "enthalpy of (saturated) water", "enthalpy of evaporation" and "enthalpy of saturated steam" respectively. Similarly the term total heat of superheated steam is now known as "enthalpy of superheated steam". Enthalpy of evaporation is the difference between enthalpy of dry saturated steam and enthalpy of water. [In enthalpy the pressure should be constant]  $\Delta H = \Delta E + P\Delta V$

Enthalpy of water The amount of heat absorbed by one kilogram of water in being heated from the freezing point ( $0^\circ C$ ) to the boiling point is known as the enthalpy of the saturated water and is denoted by the symbol  $h$ .

Enthalpy of evaporation The enthalpy of evaporation is defined as the amount of heat required to convert one kilogram of water at a given temperature  $t_s$  and pressure  $p$  into steam at same temperature and pressure.

Enthalpy of dry saturated steam It is the sum of enthalpy of saturated water and enthalpy of evaporation and is defined as the quantity of heat required to raise the temperature of one kilogram of water from freezing point to the temperature of evaporation  $t_s$  and then convert it to the dry saturated steam at that temperature and pressure.

It is denoted by the symbol  $H_s$ . The enthalpy of one kg of dry saturated steam,  $H_s$  = enthalpy of (saturated) water + enthalpy of evaporation. ( $H_s = h + L \text{ kJ/kg}$ )

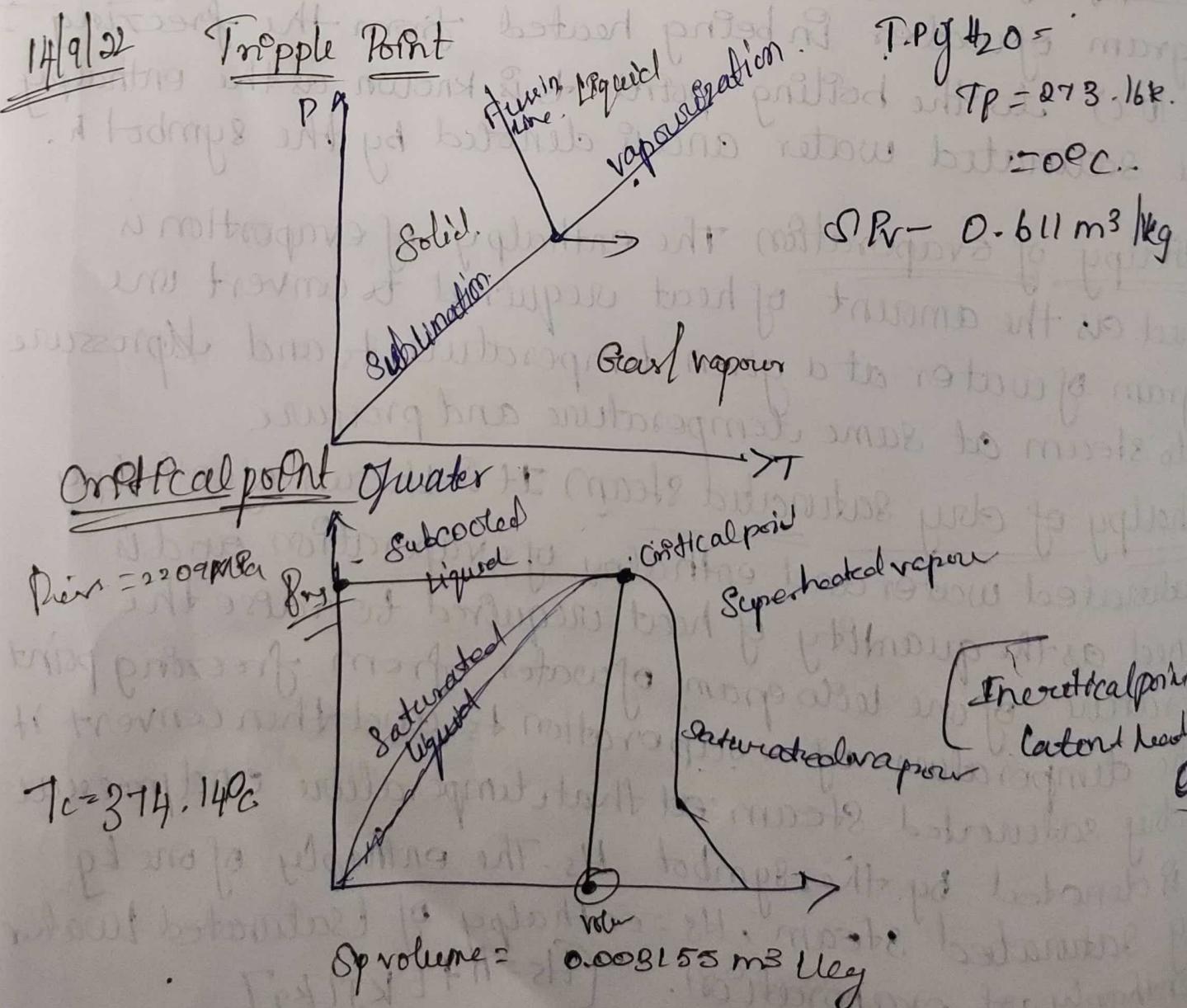
Wet steam The steam in the steam space of a boiler generally contains water mixed with it in the form of mist. Such a steam is termed as wet steam. The quality of steam as regards its dryness is termed as dryness fraction. Dryness fraction is usually expressed by the symbol  $x$ . Dryness fraction is often spoken as the quality of wet steam.

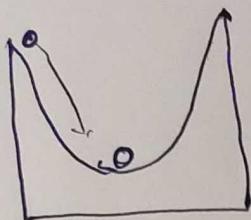
$m_s \rightarrow$  mass of dry steam contained in the steam considered and.

$m =$  mass of water in suspension in the steam considered

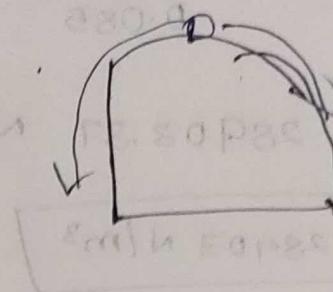
Dryness fraction

$$x = \frac{m_s}{m_s + m} \quad \rightarrow \text{mass of steam}$$





In center they will come from any point of starting taking place.



unstable equilibrium

### Stable equilibrium

Latent heat  $\rightarrow$  Temperature Increase constant volume change

Sensible heat  $\rightarrow$  volume constant Temperature change.

Q. 1 kg of gas expands P<sub>f</sub> constant pressure from zero point ~~0.085 m<sup>3</sup>~~ to 0.13 m<sup>3</sup>. The initial temperature of the gas is 22.5°C. Find the final temperature net of heat transfer changing internal energy and pressure of gas.

Given:

$$m = 1 \text{ kg}$$

Pressure = constant

$$V_1 = 0.085 \text{ m}^3$$

$$V_2 = 0.13 \text{ m}^3$$

$$T_1 = 22.5^\circ\text{C} \Rightarrow T_2 = 295.5^\circ\text{K}$$

To find,  $P_1, Q, \Delta U, T_2$

(i) Pressure

$$PV = MRT$$

$$P = \frac{MRT}{V}$$

$$W + D = n\Delta$$

$$\Delta = \Delta Q$$

$$P = \frac{1 \times 8.314 \times 295}{0.085}$$

2456.7

$$P = 28903.37 \text{ N/m}^2$$

$$P \approx 28903 \text{ N/m}^3$$

(iii) Work done:

$$WD = P \Delta V$$

$$= P(v_2 - v_1)$$

$$= 28903 (0.013 - 0.085)$$

$$= 1300.63 \text{ Joules}$$

[Some energy is lost (-)]

$$WD = -1300.63 \text{ Joules}$$

(iii) Net Heat Transfer

$$Q = W \rightarrow \text{actual formula.}$$

[Some heat is lost.

heat energy is into negative work]

$$Q = -W$$

$$Q = -(-1300.63 \text{ J})$$

$$Q = 1300.63 \text{ J}$$

(iv) Change In Internal Energy

$$\Delta U = Q + W$$

$$\Delta U = 0$$

[1st law of thermodynamics]

(+) is two formula then

(V)  $T_2 \rightarrow$  Final temperature.

At 1. Pressure = constant

$$V \propto T$$

$$V = T$$

$$\frac{V_1}{V_2} = \frac{T_1}{T_2}$$

$$\Rightarrow \frac{V_1}{T_1} = \frac{V_2}{T_2}$$

$$\frac{0.085}{295.5} \neq \frac{0.13}{T_2}$$

$$T_2 = \frac{V_2 \times T_1}{V_1}$$

$$= \frac{0.13 \times 295.5}{0.085}$$
$$= 451.94 \text{ K}$$

$$T_2 = 178.94^\circ\text{C}$$

(V)  $V_2 = V_1$  expands (b)

7.1 (a)

NA (c)

NA (d)

(V)  $V_2 = V_1$  (e)

, P2 = V<sub>2</sub>

28164

7.1 (f)

$$\frac{1.18 \times 118.8 \times 2}{100} = N$$

$$\Delta m_{PH-H} = 1 \text{ V}$$

$$(451.94 - 273)$$

$$= 178.94$$

② 5 kg of air at  $40^\circ\text{C}$  and 1 bar is heated in a ~~constant~~ <sup>adiabatic</sup> unfollow constant pressure until the volume is double so find (A) change in the volume, (B) work done (C) change in internal energy (D) change in enthalpy.

Given :  $M = 5 \text{ kg}$

$$T_1 = 40^\circ\text{C}$$

$$= 313 \text{ K}$$

$$V_1 = 2V_2 = V_2$$

$$P_1 = 1 \text{ bar} = 100 \text{ Nm}^2$$

To find

(a) change in  $V = V_2 - V_1$

(b)  $W?$

(c)  $\Delta U$

(d)  $\Delta H$

(i)  $V_2 - V_1$

$$P_1 V = mRT_1$$

$$V_1 = \frac{mRT_1}{P_1}$$

$$V_1 = \frac{5 \times 8314 \times 313}{100}$$

$$V_1 = 4.49 \text{ m}^3$$

$$\begin{aligned} V_1 &= 2V_1 \\ &= 4.49 \times 2 \\ V_2 &= 8.98 \text{ m}^3 \end{aligned}$$

(ii) Work done

$$W = P\Delta V = P(V_2 - V_1)$$

$$= 100(4.49)$$

$$W = 449 \text{ kJ}$$

(iii) Change in temperature

$$\Delta U = mC_V \Delta T$$

$$= 5 \times 0.718 \times (T_2 - T_1)$$

$C_V \rightarrow$  specific heat @  
constant volume

$C_V$  value is constant  
 $C_V$  value for air  
 $= 0.718 \text{ kJ/kg}$

# Energy Balance

Energy entering + heat entering <sub>cv</sub> = Energy leaving <sub>the c.v.</sub>

the c.v.

+ Work transfer + stored energy

(P → specific heat @ constant Pressure)

$$M_1 \left( P_1 v_1 + \frac{c_1^2}{2} + z_1 g + u_1 \right) + Q = M_2 \left( P_2 v_2 + \frac{c_2^2}{2} + z_2 g + u_2 \right) + W$$

$$M_1 = M_2 = M$$

$$m \left( u_1 + P_1 v_1 + \frac{c_1^2}{2} + z_1 g \right) + Q = m \left( u_2 + P_2 v_2 + \frac{c_2^2}{2} + z_2 g \right) + W$$

$$h = u + Pv$$

$$m \left( h_1 + \frac{c_1^2}{2} + z_1 g \right) + Q = m \left( h_2 + \frac{c_2^2}{2} + z_2 g \right) + W$$

steady flow  
energy equat.

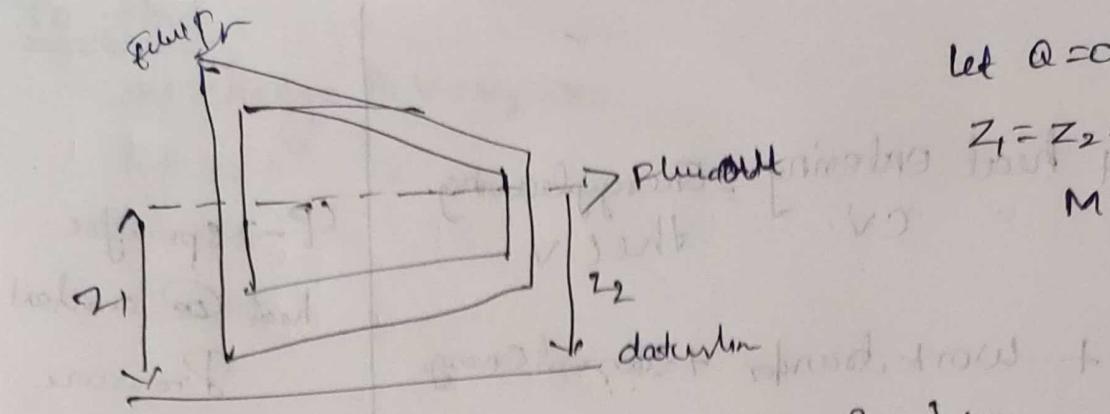
$$h_1 + \frac{c_1^2}{2} + z_1 g + \frac{Q}{m} = h_2 + \frac{c_2^2}{2} + z_2 g + \frac{W}{m}$$

$$h_1 + \frac{c_1^2}{2} + z_1 g + q = h_2 + \frac{c_2^2}{2} + z_2 g + w$$

$$q - w = h_2 - h_1 + \frac{c_2^2 - c_1^2}{2} + (z_2 - z_1)g$$

constant volume

constant density = constant mass



let  $\alpha = 0$

$$z_1 = z_2 = 0 \quad W = 0$$

$$M_1 = m_2$$

$$m \left( h_1 + \frac{c_1^2}{2} + \rho g \right) + 0 = m \left( h_2 + \frac{c_2^2}{2} + \rho g \right) + 0$$

$$\Rightarrow h_1 + \frac{c_1^2}{2} = h_2 + \frac{c_2^2}{2}$$

$$h_1 - h_2 = \frac{c_2^2 - c_1^2}{2}$$

$$M = \rho M = 1 M$$

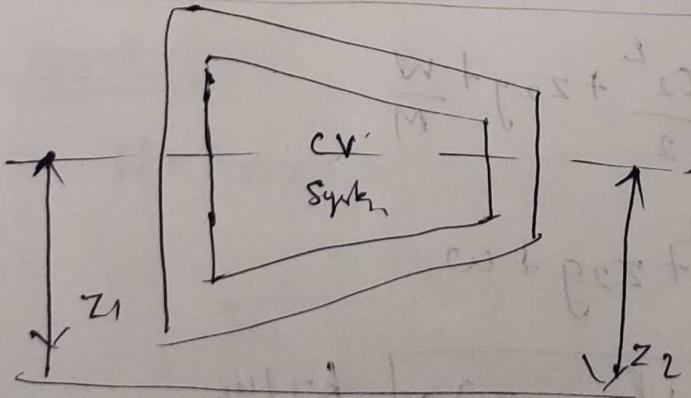
$$2(h_1 - h_2) = c_2^2 - c_1^2$$

$$\sqrt{2(h_1 - h_2)^2 + c_1^2} = c_2$$

$$c_2 > c_1 \Rightarrow c_1 = 0$$

$$\sqrt{2(h_1 - h_2)} = c$$

$$\sqrt{h_1 - h_2}$$



$$z_1 = z_2 = 0 \quad Q = 0$$

$$c_1 = c_2 = 0$$

$$\omega = \text{dreh}$$

$$m \left( h_1 + \frac{c_1^2}{2} + z_1 g \right) + Q = m \left( h_2 + \frac{c_2^2}{2} + z_2 g \right) + \omega$$

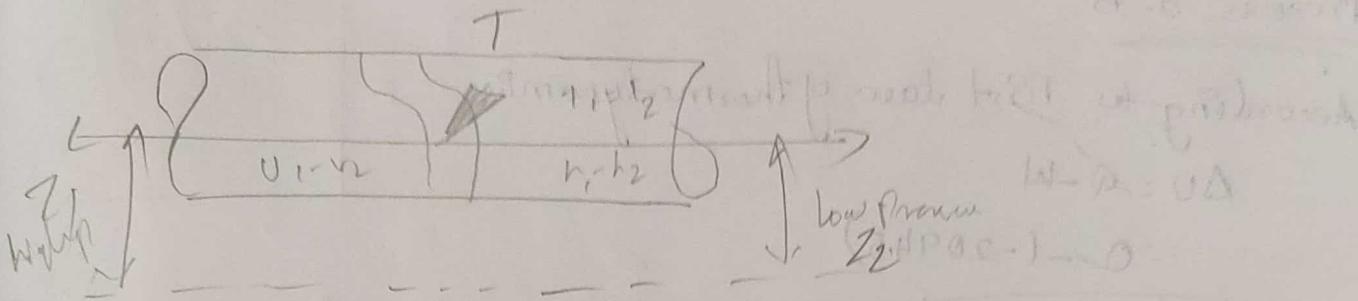
$$mh_1 = mb_2 + \omega$$

$$\omega = mh_1 - mb_2$$

$$\omega = 2m(h_1 - h_2)$$

Cochere h, z, d, w

## Throttling device



$$\Delta PE = 0$$

$$\Delta KE = 0$$

$$N, Q = 0$$

$$\boxed{h_1 = h_2}$$

$$M_1 = M_2 = M$$

$$\cancel{CPT_1 = CPT_2}$$

$$\boxed{T_1 = T_2}$$

- ① A fluid system undergoes process a-b, b-c, c-d and d-a to complete a cycle during one cycle; the total negative heat transfer is 84 kJ. The system completes 100 cycles per minute. The energy transfers are tabulated below. Estimate the amount of work done (kJw)

Process	$Q$ (kJ/m³)	$W$ (kJ/m³)	$W_{\text{av}}$ (kJ/min)
a-b	0.01 - 0	-20945	? 20945
b-c	20945	0	? 20945
c-d	2094	~35000	37700
d-a	?	?	?

Soln : Given:

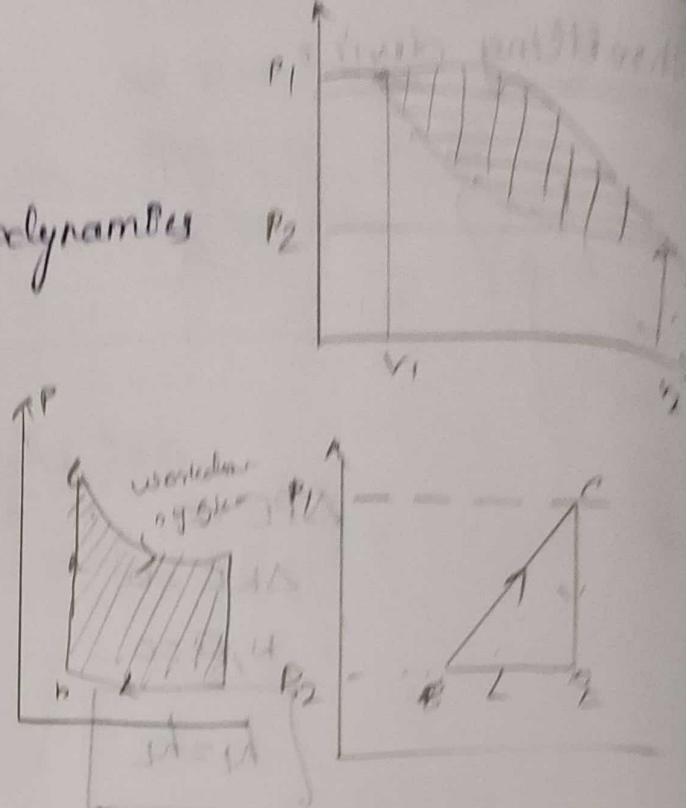
① Process a-b

According to first law of thermodynamics

$$\Delta U = Q - W$$

$$= 0 - (-20945)$$

$$\boxed{\Delta U = 20945 \text{ kJ/m}^3}$$



(ii) Process d-a

$\Sigma Q = (\text{Total heat transfer}) \times \text{NO}$   
of cycles

$$= -84 \times 100$$

$$\boxed{\Sigma Q = -8400 \text{ kJ/min}}$$

workdone by the system  
heat absorbed  
by the system

$$\Sigma Q = Q_{a-b} + Q_{b-c} + Q_{c-d} + Q_{d-a}$$

$$\boxed{Q_{d-a} = -81439 \text{ kJ/min}}$$

$$\Sigma Q = \Sigma W$$

$$-8400 = \Sigma W$$

Ans.

$$W_{d-a} = 48151 \text{ kJ/min}$$

Amount of workdone

$$\Sigma W = -8400 \text{ kJ/min}$$

watts - J/sec

$$= \frac{-8400}{1000 \times 60} \times 60$$

$$= -0.14 \text{ N} \times 1000$$

$$= -140 \text{ kW}$$

Soln : Given:

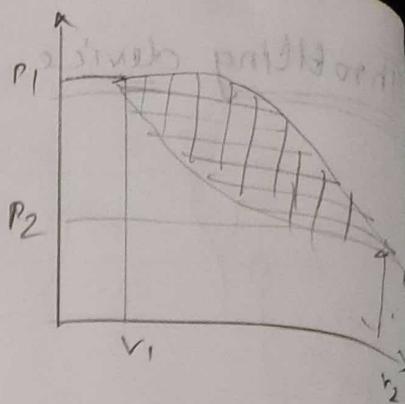
① Process a-b

According to First law of thermodynamics

$$\Delta U = Q - W$$

$$= 0 - (-20945)$$

$$\boxed{\Delta U = 20945 \text{ kJ/m}^3}$$

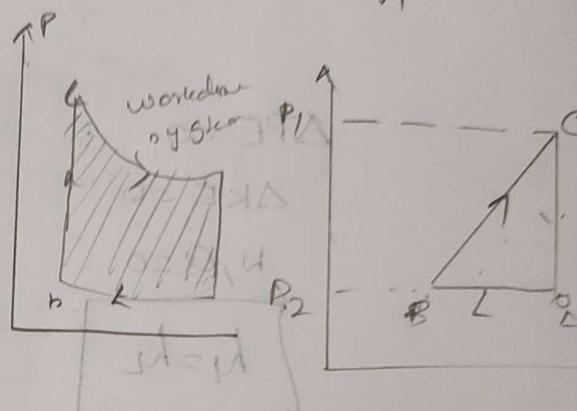


(ii) Process d-a

$\Sigma Q = (\text{Total heat transfer}) \times \text{No}$   
of cycles

$$= -84 \times 100$$

$$\boxed{\Sigma Q = -8400 \text{ kJ/min}}$$



Work done by the system  $\Rightarrow$   
Heat absorbed  
by the system

$$\Sigma Q = Q_{a-b} + Q_{b-c} + Q_{c-d} + Q_{d-a}$$

$$\boxed{Q_{d-a} = -31439 \text{ kJ/min}}$$

$$\Sigma Q = \Sigma W$$

$$-8400 = \Sigma W$$

~~W~~  
~~area~~

$$W_{d-a} = 48151 \text{ kJ/min}$$

Amount of workdone

$$\Sigma W = -8400 \text{ kJ/min}$$

Watts  $\rightarrow \text{J/sec}$

$$= \frac{-8400}{1000 \times 60} \text{ kW}$$

$$= -0.14 \text{ N/mm}^2$$

$$\boxed{= -140 \text{ kW}}$$